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2018-01

Kuai , L , Kan , E , Cao , W , Huttula , M , Ollikkala , S , Ahopelto , T , Honkanen , A-P ,
Huotari , S , Wang , W & Geng , B 2018 , ' Mesoporous LaMnO₃+delta perovskite from
spray - pyrolysis with superior performance for oxygen reduction reaction and Zn - air battery
' , Nano Energy , vol. 43 , pp. 81-90 . <https://doi.org/10.1016/j.nanoen.2017.11.018>

<http://hdl.handle.net/10138/306781>

<https://doi.org/10.1016/j.nanoen.2017.11.018>

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PII: S2211-2855(17)30694-8
DOI: <https://doi.org/10.1016/j.nanoen.2017.11.018>
Reference: NANOEN2319

To appear in: *Nano Energy*

Received date: 15 October 2017
Revised date: 4 November 2017
Accepted date: 7 November 2017

Cite this article as: Long Kuai, Erjie Kan, Wei Cao, Marko Huttula, Sami Ollikkala, Taru Ahopelto, Ari-Pekka Honkanen, Simo Huotari, Wenhai Wang and Baoyou Geng, Mesoporous $\text{LaMnO}_{3+\delta}$ perovskite from spray-pyrolysis with superior performance for oxygen reduction reaction and Zn-air battery, *Nano Energy*, <https://doi.org/10.1016/j.nanoen.2017.11.018>

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Mesoporous $\text{LaMnO}_{3+\delta}$ perovskite from spray-pyrolysis with superior performance for oxygen reduction reaction and Zn–air battery

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Abstract

Oxygen reduction reaction (ORR) is the key reaction in various electrochemical energy devices. This work reports an inexpensive mesoporous $\text{LaMnO}_{3+\delta}$ perovskite for ORR with remarkable activity, synthesized by a facile aerosol-spray assisted approach. The mesoporous $\text{LaMnO}_{3+\delta}$ material shows a factor of 3.1 higher activity (at 0.9 V vs. RHE) than LaMnO_3 obtained from co-precipitation method (LMO-CP).

Based on results of x-ray absorption near-edge spectroscopy (XANES), x-ray photoelectron spectroscopy (XPS) and Brunauer–Emmett–Teller (BET) analysis, we conclude that the chemical state of surface Mn and the high surface area are the sources to the notably enhanced activity. The study of Zn-air batteries device further confirmed a Pt/C comparable performance in the practical devices with the novel mesoporous $\text{LaMnO}_{3+\delta}$ catalyst, where the power density at 200 mA/cm^2 is only 2.1% lower than in the battery with same-loaded Pt/C catalyst. Therefore, the high mass activity and low-cost of Mn/La may make $\text{LaMnO}_{3+\delta}$ further approach to the application of electrochemical devices.

Graphical abstract

A device-feasible and Earth-abundant $\text{LaMnO}_{3+\delta}$ electrocatalyst is obtained for ORR and Zn-air batteries. Contributed by the surface oxidation state of Mn and high specific surface area, it displayed a commercial Pt/C comparable performance.

Keywords: $\text{LaMnO}_{3+\delta}$; mesoporous; oxidation state; oxygen reduction reaction; Zn-air battery

1. Introduction

Driven by the increasing environmental and energy-related problems, there is a considerable interest in novel sustainable and green power sources[1,2]. Due to the environment-friendly power generation form and high energy/power density, the

electrochemical energy devices, such as polymer electrolyte membrane fuel cells and rechargeable metal-air batteries, have attracted the widespread attention of scientists[3,4]. Oxygen reduction reaction (ORR), the cathodic process of electrochemical energy cells, determines the overall device performance due to its sluggish 4e pathway and high reaction barriers[5-7]. In general, precious Pt group (PG) catalysts are demanded to obtain high ORR kinetics[8,9]. Limited by their high cost and ultra-low abundance on Earth, scientists are therefore doing their best to search for inexpensive catalysts with a performance that would approach that of PG catalysts, and many excellent candidates have been investigated. Typically, heteroatom-doped carbon nanomaterials[10-15], metal oxides/N-rGO hybrids[16-19], transition metal carbide/heteroatom-doped carbon[20,21], and perovskites[22-29] have been extensively studied during the recent years.

Among the non-Pt group (NPG) catalysts, perovskites (ABO_3) with high conductivity have gained much attention since they were found to possess excellent intrinsic activity for oxygen catalysis[24,30], typically for $\text{LaMnO}_{3+\delta}$ that has the currently most comparable intrinsic activity to the commercial Pt/C catalyst. It is well known that the apparent ORR activity of $\text{LaMnO}_{3+\delta}$ is highly sensitive to the preparation method relative to both the state of Mn and specific surface area[28-30]. For example, the conventional solid-state reaction with high reaction temperature always leads to the particles' size as large as hundreds of nanometers[30-34], which results in an inferior apparent activity less than 1.0 A/g (at 0.9 V vs. RHE), although the materials have a high intrinsic activity. Other routes like the co-precipitation

method has been developed to efficiently prepare perovskite nanoparticles with surface area of 5~30 m²/g[35,36]. Unfortunately, the products are mainly of a lower-active phase and the apparent activity also remains low level. Currently, the apparent activity of LaMnO_{3+δ} catalysts is still far from the commercial Pt/C level. Therefore, it is still desirable to prepare nanosized LaMnO_{3+δ} with preferred phase for high efficiency ORR.

In this work, we present a mesoporous LaMnO_{3+δ} catalyst with commercial Pt/C comparable performance by an efficient nitrate spray-pyrolysis method (NSPM). The as-obtained mesoporous LaMnO_{3+δ} shows a preferred rhombohedral phase with a dominant surface Mn⁴⁺ fraction and a high specific surface area of 24.8 m²/g, which contributes a factor of 3.1 higher activity than that of LaMnO₃ nanoparticles prepared by co-precipitation (LMO-CP). We confirm further with a constructed Zn-air battery device that the performance is comparable to that of Pt/C in practical devices of the mesoporous LaMnO_{3+δ} catalyst. Therefore, as an excellent NPG catalysts for ORR, the high activity and low-cost of Mn/La may make mesoporous LaMnO_{3+δ} a novel further approach for an application in electrochemical devices.

2. Experimental Section

2.1 Chemicals and Materials

All the chemicals were of analytical grade, and used as received without further purification. The metal salts, NaOH (AR), and KOH (99.99%) were bought from Aladdin. The triblock polymer Pluronic P-123 (EO₂₀PO₇₀EO₂₀) was purchased from Sigma. The Pt/C catalyst (20% Pt loading) and Nafion (5 wt.%) solution was obtained

from Dupont Co. Ltd. The high-purity water used in this study had a resistance > 18 M Ω .

2.2 Synthesis of Porous $\text{LaMnO}_{3+\delta}$ Microspheres

The devices and method are similar to our previous work. Typically, 1 mmol $\text{Mn}(\text{NO}_3)_2$, 1 mmol $\text{La}(\text{NO}_3)_3$ and 0.25 g P123 was dissolved in 20 mL ethanol. The solution was sprayed by a household ultrasonic humidifier (1.7 MHz, 35 W). The generated mist was drawn into a glass tube in a tube furnace (67 cm, pre-heated to 480 °C) by a vacuum pump. The products were collected with a filter paper. The porous products were obtained after calcination in air at 700 °C for 4 h at a heating rate of 5 °C/min.

The porous LaNiO_3 , LaCoO_3 , and $\text{LaCo}_{0.8}\text{Fe}_{0.2}\text{O}_3$ were prepared with the same method except that the calcination temperature was 600 °C. For the synthesis of LaNiO_3 , the calcination is under O_2 (purity>99.4%) flow. $\text{La}_{0.5}\text{Sr}_{0.5}\text{CoO}_{3-\delta}$ and $\text{La}_{0.5}\text{Sr}_{0.5}\text{Co}_{0.8}\text{Fe}_{0.2}\text{O}_3$ are obtained by calcination at 800 °C.

2.3 Synthesis of LaMnO_3 Nanoparticles (LMO-CP)

The LaMnO_3 nanoparticles are prepared by a co-precipitation method.[36] 1 mmol $\text{Mn}(\text{NO}_3)_2$ and 1 mmol $\text{La}(\text{NO}_3)_3$ were dissolved in 10 mL water. 3 mL of 1.7 M NaOH solution was subsequently added. The precipitation was washed, collected, dried and finally calcined at 700 °C for 8 h in air with a heating rate of 5 °C/min.

2.4 Characterization

The samples were characterized by X-ray diffraction (XRD; Philips X'Pert with Cu $K_{\alpha 1}$ radiation ($\lambda=0.154056$ nm)), scanning electron microscopy (SEM; Hitachi S-4800) with 5 kV accelerating voltage, transmission electron microscopy (TEM) and high-resolution TEM (HRTEM) (Tecnai G2 20 S-TWIN) with 200 kV accelerating voltage. The elements' EDX mapping was performed by SEM (Hitachi S-5500) with 30 kV accelerating voltage. X-ray photoelectron spectroscopy (XPS) experiments were conducted on ESCALAB 250 (America) at 15 kV. The Brunauer–Emmett–Teller (BET) specific surface areas and Barrett–Joyner–Halenda (BJH) pore size distributions were measured and analyzed by N_2 sorption isotherms (77 K) with 3Flex Surface Characterization Analyzer (Micromeritics, America).

X-ray Absorption Spectroscopy Measurements:

The XANES measurements were performed on a home-laboratory spectrometer based on a spherically bent Si(440) and Si(531) monochromator crystals in the Johann geometry, curvature radius 500 mm.[37] The design is similar to that of Seidler et al.[38, 39] An x-ray tube with a Ag anode was used as the photon source (20 kV voltage and 2 mA current for Co K edge, and 9 kV/10 mA for the Mn K edge). The monochromated x-rays were focused on a powder sample in front of a NaI scintillator detector. The detector and monochomator followed the Rowland circle with linear translation motors and a goniometer for the selection of the Bragg angle.

Electrode Preparation and ORR Measurements:

The glassy carbon electrode (5 mm in diameter, Pine Instrument) was polished with first 1- μm and then 0.05- μm particle-sized Al_2O_3 powders. The catalyst ink was prepared by mixing 5 mg catalyst powder, 1 mg carbon (Vucan XC-72, Carbot), 10 μL of 5 wt.% Nafion (Dupont), 0.66 mL H_2O and 0.34 mL dimethylformamide (DMF) with assistance of ultrasonic treatment for 5 minutes. 10 μL of the catalytic ink was dropped onto the polished glassy carbon electrode and dried naturally. The catalyst loading was 0.25 mg cm^{-2} . For the carbon black modified electrodes, the mass loading was 0.05 mg cm^{-2} . The electrodes with catalyst loadings of 0.125 and 0.05 mg cm^{-2} were prepared by reducing the amount of active materials.

The ORR measurements were performed in 0.1 M KOH solution by a three-electrode system with an electrochemistry workstation (CHI 660C), where the Ag/AgCl electrode (KCl saturated) was used as reference electrode, and Pt plate (1 cm*1 cm*0.02 cm) was used as counter electrode. The static cyclic voltammograms (CVs) were recorded under N_2 (purity > 99.999%) and O_2 (purity > 99.999%) saturated 150 mL of 0.1 M KOH, respectively. The rotating disk (glassy carbon) electrode measurements were performed at the rotating speeds of 400, 625, 900, 1225 and 1600 rpm (Pine Instrument rotator). The rotating ring (Pt)-disk (glassy carbon) electrode (RRDE, 37% collection efficiency, Pine) measurements were performed at the rotating speed of 1600 rpm, and the potential of ring electrode was set at 0.2 V (vs. Ag/AgCl electrode). The current-time curves were recorded at -0.5 V (vs. Ag/AgCl electrode) at a RDE rotating rate of 1225 rpm. All the scanning rates were 10 mV/s.

The potential was iR-corrected and referenced to reversible hydrogen electrode (RHE), which was calibrated with the peak position of Mn sites in the literature. Consequently, $E_{\text{RHE}} = E_{\text{applied}} + 0.960 - iR$, where E_{applied} is the applied potential vs. Ag/AgCl electrode and R stands for the Ohm resistance determined by electrochemical impedance spectrum ($\sim 43 \Omega$ in this work, **Fig. S1**). In this work, dual references (Ag/AgCl and RHE) to potential are presented to facilitate the comparison with the result with existing literature, and all the potentials in the results discussion are referenced to RHE except when mentioned specifically.

Zn-Air Battery Assembly and Test:

A home-built Zn-air battery was assembled with a Zn plate with diameter of 1.5 cm as an anode, a catalyst-modified gas diffusion electrode (GDE, PTFE-treated hydrophobic carbon paper) with active area of about 1.0 cm^2 as the cathode, and a filter paper as a separator. About 0.3 mL of 6.0 M KOH solution was added into the cell as the electrolyte. A metal net was covered on the GDE as the cathode current collector. The loading of active materials in GDEs for all the batteries was about 2 mg/cm^2 . For the oxide catalysts, 0.5 mg/cm^2 of carbon black (Vucan XC-72, Carbot) was added to increase the conductivity. The resistance of the cell was about 0.8Ω . The cell measurements were performed under the O_2 flow with the temperature of about 20°C .

3. Results and Discussion

3.1 Synthesis and Characterizations

The synthesis procedure of mesoporous $\text{LaMnO}_{3+\delta}$ microspheres consists of amorphous precursor preparation and subsequent calcination process. Firstly, the amorphous LaMnO_3 precursor was prepared by NSPM as reported in our previous work [40,41]. As illustrated in **Fig. 1a**, the NSPM process consists of spraying the mother solution (part i, containing $\text{Mn}(\text{NO}_3)_2$, $\text{La}(\text{NO}_3)_3$ and Pluronic P-123 ($\text{EO}_{20}\text{PO}_{70}\text{EO}_{20}$)), pyrolysis of nitrates (part ii), and powder collection (part iii). Finally, the mesoporous $\text{LaMnO}_{3+\delta}$ microspheres were obtained by thermal treatment. As shown in the scanning electron microscopy (SEM) image (**Fig. 1b**), the amorphous LaMnO_3 microspheres with sizes of $0.886 \pm 0.300 \mu\text{m}$ are solid and surface-smooth. After calcination for removal of P-123 template, the obtained $\text{LaMnO}_{3+\delta}$ products exhibit typical porous structures with sizes of $0.716 \pm 0.310 \mu\text{m}$ (**Fig. 1c**). The transmission electron microscopy (TEM) image (**Fig. 1d**) further presents the detailed porous structure information. The microspheres are assembled by nanoparticles with sizes of 35–60 nm. The pore sizes ranged from 20 to 50 nm. Based on the N_2 adsorption-desorption isotherm measurement (**Fig. S2a**), the mesoporous $\text{LaMnO}_{3+\delta}$ products have a high Brunauer–Emmett–Teller (BET) specific surface area of $24.8 \text{ m}^2/\text{g}$ and Barrett-Joyner-Halenda (BJH) pore size centered at $\sim 30 \text{ nm}$ (**Fig. S2b**), favorable for catalytic active site exposure. Successively, the high-resolution TEM (HRTEM) image (**Fig. 1e**) shows the lattice spacing of 0.29 nm, which can be indexed to the {110} plane. Moreover, the energy-dispersive X-ray

(EDX) elemental mapping (**Fig. 1f**) confirms the presence of O, Mn and La elements. Importantly, the O (green), Mn (white) and La (red) elements are found to be well overlapped with each other, suggesting the uniform distribution of Mn and La in $\text{LaMnO}_{3+\delta}$. In addition, some other mesoporous perovskite oxides were also prepared by NSPM in this work for meaningful comparison, such as LaCoO_3 (LCO), LaNiO_3 (LNO), $\text{La}_{0.5}\text{Sr}_{0.5}\text{CoO}_{3-\delta}$ (LSCO), *etc.* (**Fig. S3**)

X-ray powder diffraction (XRD) patterns were performed to analyze the crystalline phase of products. As show in **Fig. 2a**, only perovskite phase (black) with low crystallization degree was observed when LaMnO_3 precursor was calcined at 600 °C for 4 h. When the temperature was increased to 700 °C, the well-crystallized $\text{LaMnO}_{3+\delta}$ products were obtained (blue). It is interesting that the obtained sample is rhombohedral phase (green, JCPDS NO. 50-299), which is the preferred phase for ORR [29]. Several diffraction peaks split into two peaks (the dashed box) and one weak peak centered at 2θ of 38.5° appears (insets). For meaningful comparison, we also prepared the LaMnO_3 nanoparticles by co-precipitation (marked as LMO-CP)[36]. The obtained LMO-CP possesses particle sizes 40–70 nm (**Fig. S4a, b**) and BET specific surface area of 16.4 m²/g (**Fig. S4c**). Different from the mesoporous $\text{LaMnO}_{3+\delta}$ from NSPM, the LMO-CP presents cubic phase (red), and neither peak centered at 2θ of about 38.5° nor obvious peak splitting can be observed through its XRD pattern. The XRD patterns of other products obtained from NSPM are also confirmed to be perovskite structure (**Fig. S5**) after calcination.

The Mn K-edge x-ray absorption near edge structures (XANES) were investigated to elucidate the differences in the synthetic samples. The XANES spectra of the mesoporous $\text{LaMnO}_{3+\delta}$ (blue) and LMO-CP (red) are depicted in **Fig. 2b** along with those from the MnO (black), Mn_3O_4 (green), and MnO_2 (orange) for comparison purposes. In general, the XANES of the $\text{LaMnO}_{3+\delta}$ resembles the one of the LaMnO_3 , with clear features of the pre-edge bump at ~6540 eV, white line at 6557 eV, and a post-edge bump at 6568 eV. The white line positions of the two samples stay between these of MnO and Mn_3O_4 , but much lower in energy than the one from MnO_2 , which is consistent to the perovskite phase. No obvious energy shift was found between the samples, indicating a similar Mn oxidation state in the bulk. However, obvious differences are seen at the width of the white line and the height of the pre-edge bumps. Narrowing the main peak refers to the asymmetrisation of the Mn 4p orbital caused by the rhombohedral phase in the $\text{LaMnO}_{3+\delta}$ rather than the cubic phased matrix, in line with previously reported first-principles evaluations on similar systems [42]. Interestingly, the signature of the e_g states and its changes can be identified in the K-edge XANES. In the inset of Fig. 2b, clear changes of the pre-edge ‘bump’ intensity can be seen. This ‘bump’ bears the hybridizations of the 4p orbitals to the 3d orbitals of the Mn neighboring atoms, yet populating the 3d partial density of states, and associating to the transition to the e_g states [43]. Compared with the LMO-CP, slight decrease of the pump intensity is found in the $\text{LaMnO}_{3+\delta}$, indicating the higher e_g occupancy. The $\text{LaMnO}_{3+\delta}$ exhibit much higher activity than that of LMO-CP,

which dissatisfies the result on e_g electron indicator. Thus, the state of surface Mn may play more dominant role in the ORR process, which will be discussed later.

X-ray photoelectron spectra (XPS, **Fig. 2c, d** and **S6a**) were measured to confirm and compare the surface chemical environment of the as-prepared $\text{LaMnO}_{3+\delta}$ and LMO-CP samples. As shown in the left of **Fig. 2c** with C1s as internal standard (**Fig. S6b**) of binding energy (E_b), the binding energy (E_b) peak of Mn2p in rhombohedral $\text{LaMnO}_{3+\delta}$ (642.13 eV) is positively shifted by 0.44 eV compared with LMO-CP (641.69 eV), indicating the higher surface oxidation state of Mn in $\text{LaMnO}_{3+\delta}$, which is different from that in the bulk determined by XANES. This is not surprising since the effective detection depth of the XPS allows only a surface-state probation while the hard X-rays measures the bulk of the powders. The surface oxygen spectra (right of **Fig. 2c**) further clarify this. The peaks centered at the lower $E_b^{\text{O}1s}$ are assigned to the lattice O and the ones centered at the higher $E_b^{\text{O}1s}$ are corresponded to $-\text{OH}$ [44]. Firstly, there is only a slight $E_b^{\text{O}1s}$ difference (0.08 eV) of $-\text{OH}$ because the Pauling's electronegativity of H (2.20) is much larger than the electronegativity difference of Mn between $\text{LaMnO}_{3+\delta}$ and LMO-CP. While, the $E_b^{\text{O}1s}$ peak for lattice O of $\text{LaMnO}_{3+\delta}$ (529.50 eV) is positively shifted by extraordinary 0.52 eV than that of LMO-CP (528.98 eV). Moreover, the $E_b^{\text{O}1s}$ peak for lattice O of $\text{LaMnO}_{3+\delta}$ falls in the region between the E_b peak in LaMnO_3 (~529 eV) [45] and MnO_2 (530 eV) [34]. Successively, we made an assignment of the peaks for various oxidation states of surface Mn by fitting the Mn2p spectra (**Fig. 2d** and **Table S1**). As a result, the $\text{LaMnO}_{3+\delta}$ possesses a higher proportion of Mn^{IV} (43.4%, left of **Fig. 2d**) than

LMO-CP (31.0%, right of **Fig. 2d**). Besides, consistent with the previous reports[46], the surface segregation of La_2O_3 was also found in the two products where XPS (**Table S2**) shows that the surface Mn/La ratio is 0.54 and 0.78 in $\text{LaMnO}_{3+\delta}$ and LMO-CP, respectively. The larger La_2O_3 segregation in rhombohedral $\text{LaMnO}_{3+\delta}$ surface may be responsible for the larger surface Mn^{4+} proportion.

3.2 Electrocatalytic Performance toward ORR in Alkaline Media

The electrocatalytic activity of the mesoporous $\text{LaMnO}_{3+\delta}$ and LMO-CP toward ORR was evaluated in an O_2 -saturated 0.1 M KOH solution. The carbon black and commercial Pt/C catalysts with identical electrochemical active surface area of $46.0 \text{ m}^2/\text{g}$ (**Fig. S7**) were also investigated for meaningful comparison. Besides, several repeated measurements with graphite rod instead of Pt plate as counter electrode were also performed to exclude the possible effect of counter electrode on the results (**Fig. S8**). As displayed in **Fig. 3a**, obvious O_2 reduction peaks are found for all these samples. As presented in **Table 1**, the ORR peak for $\text{LaMnO}_{3+\delta}$ (red) is centered at 0.872 V with peak current density (j_p) of $0.75 \text{ mA}/\text{cm}^2$, which is 27 mV higher than LMO-CP (pink, 0.845 V with j_p of $0.57 \text{ mA}/\text{cm}^2$). Furthermore, the activity of $\text{LaMnO}_{3+\delta}$ is even comparable to the same mass-loaded commercial Pt/C catalyst, whose peak potential is just 25 mV lower than that of Pt/C (green, 0.897 V). Successively, the ORR polarization curves on rotating disk electrode (RDE) (**Fig. 3b**) were recorded at a rotating speed of 1600 rpm. Herein, all the ORR polarization curves have been corrected by removing the background currents that measured under the N_2 -saturated electrolyte. We also present the ORR polarization of carbon black,

which suggests that the activity of carbon black (blue) used in catalyst ink can be negligible for discussing the activity of oxides. Apart from the carbon black, all the limiting current densities (j_L) of porous $\text{LaMnO}_{3+\delta}$ (red), LMO-CP (pink) and Pt/C catalysts (green) are highly close to the theoretical j_L (5.75 mA/cm^2 at 1600 rpm), indicating a near 4e ORR pathway. While, the half-wave potential ($E_{1/2}$) for the porous $\text{LaMnO}_{3+\delta}$ ($E_{1/2} = 0.852 \text{ V}$) is 50 mV positive than LMO-CP ($E_{1/2} = 0.802 \text{ V}$). Moreover, the activity of porous $\text{LaMnO}_{3+\delta}$ is highly approaching to that of the same-loaded commercial Pt/C catalyst: The $E_{1/2}$ for the porous $\text{LaMnO}_{3+\delta}$ is just 36 mV lower than Pt/C, further indicating a superior ORR catalytic activity of $\text{LaMnO}_{3+\delta}$ with relatively low cost. Besides, we also studied the ORR electrocatalytic performance of the as-prepared porous LaNiO_3 and LaCoO_3 . However, their activity is far worse than that of the $\text{LaMnO}_{3+\delta}$ (**Fig. S9**) in the same condition.

The electron transfer number (n), directly associated with the ORR pathway, is used to evaluate the ORR efficiency. The Koutecky-Levich equation [47,48] (Eq. (1) and (2)) is used to estimate the n value.

$$\bar{j}^{-1} = j_k^{-1} + j_d^{-1} \quad (1)$$

$$j_d = 0.62nFC_0D_0^{2/3}\nu^{-1/6}\omega^{1/2} \quad (2)$$

In the Koutecky-Levich equation, the j is the measured Faradic current density, j_k is the kinetic-limiting current density, j_d is the diffusion-limiting current at the RDE rotating speed of ω (rad/s), n is the transferred electron number, F is the Faraday constant (96485 C), C_0 is the bulk concentration of dissolved O_2 (1.21 mol/m^3 in 0.1 M KOH), D_0 is O_2 diffusion coefficient ($1.87 \times 10^{-9} \text{ m}^2/\text{s}$ in 0.1 M KOH), ν is

kinematic viscosity of electrolyte ($1 \times 10^{-6} \text{ m}^2/\text{s}$ for 0.1 M KOH) and ω is the angular frequency of RDE rotation. Given the above conditions, there is a linear relationship between j^{-1} and $\omega^{-1/2}$. **Fig. 3c** shows the Koutecky-Levich analysis of the j with different rotation rates of 400, 625, 900, 1225 and 1600 rpm (**Fig. S10**) at 0.5 V. When performing the Koutecky-Levich analysis, the Faradic j was corrected by the removal of background current measured under N_2 atmosphere (the black lines in **Fig. S10**). According to the Koutecky-Levich equation, the slope of j^{-1} function of $\omega^{-1/2}$ is associated with the n value of ORR process. The slopes of mesoporous $\text{LaMnO}_{3+\delta}$, LMO-CP and Pt/C catalysts are calculated to be 2.201 ± 0.014 , 2.265 ± 0.017 and $2.176 \pm 0.024 \text{ cm}^2 \text{ mA}^{-1} \text{ s}^{-1/2}$. Given the n value for Pt/C is 4, the n values for $\text{LaMnO}_{3+\delta}$ and LMO-CP is 3.95 and 3.84, indicating the 4e pathway for both mesoporous $\text{LaMnO}_{3+\delta}$ catalyst and LMO-CP.

To discuss the mass activity and intrinsic activity of mesoporous $\text{LaMnO}_{3+\delta}$ and LMO-CP, an electrocatalysis with different catalyst loadings was performed (**Fig. S11**). The following activity was based on the measurements with catalysts loading of 0.05 mg cm^{-2} . First, we discuss the mass activity (j_m), which is critical to the device's performance and determined by both the intrinsic activity and specific surface area. The potential-dependent j_m plots of mesoporous $\text{LaMnO}_{3+\delta}$, LMO-CP and Pt/C catalysts are displayed in **Fig. 3d**. The j_m of Pt/C catalyst is normalized by the loading of metallic Pt ($2 \mu\text{g}$). Herein, we discuss j_m at 0.9 V (vs. RHE). The j_m of mesoporous $\text{LaMnO}_{3+\delta}$ (red) reaches extraordinary $2.83 \pm 0.20 \text{ A/g}_{\text{oxide}}$, which is 3.1 times that of LMO-CP ($0.90 \pm 0.10 \text{ A/g}_{\text{oxide}}$, pink). To the best of our knowledge, the mass activity

in this work is notably higher than the reported best values of $\text{LaMnO}_{3+\delta}$ catalysts [33, 49, 50], and it is even superior to some carbon-based materials with ultralarge specific surface areas (**Table S3**). Furthermore, it is highly worthy to mention that the j_m of $\text{LaMnO}_{3+\delta}$ has reached 4.5% of metallic Pt ($63.05 \pm 4.45 \text{ A/g}_{\text{Pt}}$, green). In general, the O_2 mass transport potential loss can be negligible when the catalyst film thickness is less than $20 \text{ }\mu\text{m}$ [51, 52]. We assume the $0.4 \text{ mg}_{\text{Pt}}/\text{cm}^2$ of Pt/C catalyst is used to generate electric power. With the mesoporous $\text{LaMnO}_{3+\delta}$, a loading of $8.9 \text{ mg}_{\text{oxide}}/\text{cm}^2$ is required to obtain the same cathode performance. Considered the density of $\sim 7 \text{ g/cm}^3$ of $\text{LaMnO}_{3+\delta}$ and 50% porosity of catalyst film [46], the corresponding catalyst film thickness is $\sim 24 \text{ }\mu\text{m}$, where the O_2 diffusion potential loss almost can be ignored. Moreover, the much more earth abundance of Mn (950 ppm) and La (32 ppm) than Pt (0.003 ppm) [48] makes mesoporous $\text{LaMnO}_{3+\delta}$ to be a potential commercial catalyst.

As for the intrinsic activity, the j was normalized by the oxides area based on the BET surface areas. Consequently, the intrinsic activity (at 0.9 V vs. RHE) of mesoporous $\text{LaMnO}_{3+\delta}$ from NSPM ($11.5 \text{ }\mu\text{A}/\text{cm}^2_{\text{oxide}}$) is 2.1-fold better than that ($5.5 \text{ }\mu\text{A}/\text{cm}^2_{\text{oxide}}$) of LMO-CP. We propose that the enhanced intrinsic activity stems from the surface state of Mn, although Shao-Horn *et al.*'s work suggest that the activity peak will appear at the e_g -filling slightly lower than 1 for $\text{LaMnO}_{3+\delta}$ according to the “volcano shape” relationship between ORR activity and e_g -filling of ABO_3 perovskites[30]. However, the present XANES results show that the e_g -filling of $\text{LaMnO}_{3+\delta}$ bulk from NSPM is comparable or even slightly higher than LMO-CP. Thus, the bulk e_g -filling contributes less dominantly compared to the surface state of

Mn because the electrocatalysis is more sensitive to the surface chemical environment instead of that in the bulk.

Beyond the activity issue, electrocatalytic stability is also a critical factor to evaluate the materials. Herein, the long-time continuous ORR tests were carried out to explore the durability of the mesoporous $\text{LaMnO}_{3+\delta}$ and Pt/C catalysts. As displayed in **Fig. 3e**, the mesoporous $\text{LaMnO}_{3+\delta}$ (red) exhibits better catalytic endurance than commercial Pt/C (black) catalyst. In addition, the catalytic endurance toward fuel crossover effect is an important factor to evaluate an ORR catalyst. Herein, we investigated the CH_3OH -tolerance of catalysts as a case study. According to the potential change after injection of absolute CH_3OH into the electrolyte solution (The final concentration of CH_3OH is 1.0 M.), as shown in **Fig. S12**, little negative shift of potential for $\text{LaMnO}_{3+\delta}$ (red) was observed after CH_3OH was introduced. This result undoubtedly suggests an excellent CH_3OH -tolerance.

3.3 RRDE Study and Potential Mechanism Discussion

The rotating ring-disk electrode (RRDE) tests were carried out to further study the ORR process of mesoporous $\text{LaMnO}_{3+\delta}$ catalyst. As shown in **Fig. 4a**, compared with the LSVs in N_2 -saturated electrolyte, the ring currents relative to peroxide (HO_2^-) yield were detected for both $\text{LaMnO}_{3+\delta}$ (red) and LMO-CP (green) catalysts along with the ORR process in O_2 -saturated electrolyte. However, the ring current is about two orders of magnitude lower than the disk current, indicating the high efficiency of ORR. The potential-dependent HO_2^- yields and n values were obtained directly from the RRDE test results based on the Eq. (3) and (4)[18, 54].

$$(\text{HO}_2^-)\% = 200 \times \frac{i_{ring}/N}{i_{disk} + i_{ring}/N} \quad (3)$$

$$n = 4 \times \frac{i_{disk}}{i_{disk} + i_{ring}/N} \quad (4)$$

Where the i_{disk} and i_{ring} are the measured Faradic currents in the corresponding disk and ring electrodes, N is the collection efficiency of ring electrode (0.37), and n is the electron transfer number. As for the calculation of n value and HO_2^- yields, both the ring and disk current are background corrected by taking off the currents measured under N_2 atmosphere. As displayed **Fig. 4b**, we can find that both n values (blue) and HO_2^- yield (pink) plots consist 3 parts. In the first potential region before 0.70 V, for both $\text{LaMnO}_{3+\delta}$ and LMO-CP, the n values are ~ 3.99 , but they are all decreased to ~ 3.95 in the part with potential lower than ~ 0.6 V. Based on the measured n values and HO_2^- yield, the ORR process on LaMnO_3 -NSPM and LMO-CP all follows the 4e pathway. As for the decreased n number in the potential lower than 0.7 V, the carbon addition may be responsible. According to Savinova *et al.*'s work [32, 33], carbon component plays an important role in the ORR process by accelerating the H_2O_2 formation, leading to the high H_2O_2 yield.

There are two couples of redox pairs in LaMnO_3 surface [55], namely, $\text{Mn}^{3+}/\text{Mn}^{4+}$ and $\text{Mn}^{2+}/\text{Mn}^{3+}$ redox couples. According to the CVs (**Fig. 3a**) of $\text{LaMnO}_{3+\delta}$ and LMO-CP under N_2 atmosphere, the conversion of Mn^{4+} to Mn^{3+} appears between 0.75 and 1.0 V, and Mn^{3+} conversion to Mn^{2+} starts at the potential after 0.7 V. The $\text{Mn}^{4+}/\text{Mn}^{3+}$ conversion peak current of mesoporous LaMnO_3 from NSPM is larger than that of LMO-CP, indicating more Mn^{4+} in $\text{LaMnO}_{3+\delta}$ surface. Meanwhile, it is at

this stage, the potential region of Mn^{4+} reduction, that the activity of $\text{LaMnO}_{3+\delta}$ surpasses that of LMO-CP rapidly. Many reports have suggested that the ORR activity of Mn-based perovskites is highly dependent of the surface Mn oxidation state [32, 46, 56]. The mixed $\text{Mn}^{3+}/\text{Mn}^{4+}$ surface is critical to obtain fast ORR kinetics. In addition, according to the XPS result suggests the $\text{LaMnO}_{3+\delta}$ from NSPM possesses more surface Mn^{4+} proportion (43.4%) than that in LMO-CP (31%). Therefore, the notably surface Mn^{4+} is the source to the higher pristine activity, which is well consistent with recent reports [46, 48].

3.4 Device Performance of Zn-air Batteries

To evaluate the feasibility and performance in a practical device using the obtained mesoporous $\text{LaMnO}_{3+\delta}$ catalyst, we built a Zn-air battery. As shown in **Fig. 5a**, the battery consists of Zn plate as anode, catalyst-modified gas diffusion electrode (GDE) as cathode, and 6.0 M KOH as electrolyte. The active area of electrode is about 1.0 cm^2 . The assembly of Zn-air batteries with commercial Pt/C and LMO-CP catalysts is the same. All the catalyst loading on the GDE for the batteries is 2.0 mg/cm^2 . For comparison, the battery with bare carbon paper as the cathode was also investigated.

Fig. 5b presents the I-V (red) and I-P (blue) plots of our batteries. As displayed in Table 1, the open-circuit voltage of cell with mesoporous $\text{LaMnO}_{3+\delta}$ catalyst is 1.43 V, which is slightly lower than that of with Pt/C (1.47 V). It is worth to mention that the cell voltages and power densities of the batteries with $\text{LaMnO}_{3+\delta}$ catalyst is highly approaching to that of with Pt/C catalyst. Moreover, the difference is still small even

the current density is increased to hundreds of milliamperes per square centimeter. For example, the power density at 200 mA/cm² is 198.6 mW/cm², which is only 2.1% lower than the battery with same-loaded Pt/C catalyst (202.8 mW/cm²). However, considering the practical application, the cost of LaMnO_{3+δ} catalyst is much lower than commercial Pt/C. As for the battery with LMO-CP catalyst, the open-circuit voltage is only 1.38 V, slightly lower than that with the LaMnO_{3+δ} catalyst. However, the voltage and power density difference are obviously larger and larger with the increase of current density. This finding is well consistent with ORR polarization study, and supports the conclusion of RRDE study that the Mn³⁺/Mn⁴⁺ redox pair is more dominant for LaMnO_{3+δ}. Besides, the performance of the cell with bare carbon paper is negligible in comparison with all the batteries with catalyst-modified cathode. Furthermore, **Fig. 5c** vividly displays the digital photos of “LMO”-shaped pattern assembled by 30 light-emitting diodes (LED, nominal power: ~30 mW), which were powered by two tandem home-made Zn-air batteries with LaMnO_{3+δ} as catalyst. A bright and continuous green emission was observed when the LEDs were powered on. Thus, the obtained LaMnO_{3+δ} catalyst can produce high device performance, such as Zn-air batteries.

4. Conclusion

In summary, we present the preparation of device-feasible non-precious mesoporous LaMnO_{3+δ} catalysts by NSPM with superior ORR activity. Contributed by the abundant surface Mn⁴⁺, a large specific surface area and mesoporous structure, the obtained mesoporous LaMnO_{3+δ} displayed is 3.1-fold better than that for the LaMnO₃

catalysts from co-precipitation method. It is a new benchmark for the LaMnO_3 -based perovskite catalysts for ORR in alkaline media. Moreover, the mass activity reaches 22.5% of commercial Pt/C catalyst and corresponding 4.5% of metallic Pt while the earth-abundance of La and Mn is 4~5 orders of magnitude higher. The device study of home-built Zn-air batteries further confirmed the feasibility and Pt/C comparable performance in the practical device using the obtained mesoporous $\text{LaMnO}_{3+\delta}$ as catalyst. This work demonstrates the feasibility of developing mesoporous $\text{LaMnO}_{3+\delta}$ materials as high efficiency ORR electrocatalysts.

Acknowledgements

This work was supported by the National Natural Science Foundation of China (21271009, 21471006), the Natural Science Foundation of Anhui Provincial Education Department (KJ2017A111), the Programs for Science and Technology Development of Anhui Province (1501021019). W. C. and M. H. acknowledge EU Regional Development Fund and Council of Oulu Region. S. O., T. A., A.-P. H. and S. H. were supported by the Academy of Finland (project 1295696).

Appendix A. Supplementary material

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Fig. 1 The synthesis procedure (a) of mesoporous $\text{LaMnO}_{3+\delta}$, SEM images of LaMnO_3 precursor (b) and mesoporous $\text{LaMnO}_{3+\delta}$ product (c), TEM (d), HRTEM (e) images, and EDX-mapping (f) of the mesoporous $\text{LaMnO}_{3+\delta}$ microspheres.

Fig. 2 (a) XRD patterns of LMO-600 (black), mesoporous $\text{LaMnO}_{3+\delta}$ (blue), LMO-CP (red) and the standard patterns of rhombohedral $\text{LaMnO}_{3.26}$ (blue) and cubic LaMnO_3 (pink); (b) Mn K-edge XANES spectra of various samples; (c) XPS Mn2p (left) and O1s (right) spectra of $\text{LaMnO}_{3+\delta}$ (gray) and LMO-CP (green); (d) Fitted XPS Mn2p spectra of $\text{LaMnO}_{3+\delta}$ (left) and LMO-CP (right).

Fig. 3 CVs (a) and LSV curves (b), Koutecky-Levich analysis (c), and potential dependent mass activity plots (d) of mesoporous $\text{LaMnO}_{3+\delta}$ (red), LMO-CP (pink) and commercial Pt/C (green) catalysts, and retention plots after long-time electrocatalysis procedure (e) of $\text{LaMnO}_{3+\delta}$ (red) and Pt/C (black) catalysts. The error bars in Figure 3c represents the standard deviations of at least 3 independent tests.

Fig. 4 RRDE tests (a) and potential-dependent peroxide yield (purple) and electron transfer numbers (n) (blue) of mesoporous $\text{LaMnO}_{3+\delta}$ and LMO-CP catalyst at the rotation rate of 1600 rpm.

Fig. 5 (a) Scheme of our home-made Zn-air batteries. (b) I-V and I-P plots of Zn-air batteries with bare, mesoporous $\text{LaMnO}_{3+\delta}$, LMO-CP and commercial Pt/C

catalysts-modified GDE. (c) Digital photos (Left: power-off under daylight; Middle: power-on under daylight; Right: power-on under dark) of “LMO” shaped light-emitting diodes powered by two tandem Zn-air batteries with $\text{LaMnO}_{3+\delta}$ as catalyst.

Table 1. A summary of ORR and Zn-air batteries' performance with $\text{LaMnO}_{3+\delta}$, LMO-CP and commercial Pt/C catalysts.

Materials	Loading mg/cm^2	E_p V	j_p mA/cm^2	$j_{m, 0.9 \text{ V}}^{[a]}$ A/g	$n_{0.9 \text{ V}}$	Voltage of Zn-air batteries V		
						V_{oc}	V $1 \text{ mA}/\text{cm}^2$	V $10 \text{ mA}/\text{cm}^2$
$\text{LaMnO}_{3+\delta}$	0.25	0.872	0.57	2.83 ± 0.20	3.99	1.430	1.322	1.255
LMO-CP	0.25	0.845	0.75	0.90 ± 0.10	3.99	1.384	1.309	1.225
Pt/C	0.25	0.897	0.64	$63.05 \pm 4.45^{[b]}$	4	1.473	1.324	1.271

[a] The mass activity was calculated with catalyst loading of 0.05 mg cm^{-2} .

[b] The j_m was normalized by the loading of metallic Pt ($10 \mu\text{g}$).

Highlights

- A device-feasible mesoporous $\text{LaMnO}_{3+\delta}$ catalysts with commercial Pt/C comparable performance was developed by a spray-pyrolysis approach for ORR and Zn-air batteries.
- It is confirmed that the surface Mn with a high Mn^{4+} proportion is positive to the ORR activity.